

Novel Methods for Reducing UHP Gas Usage in Fabs: Back Diffusion Minimization

Customized Project; Sponsored by Intel

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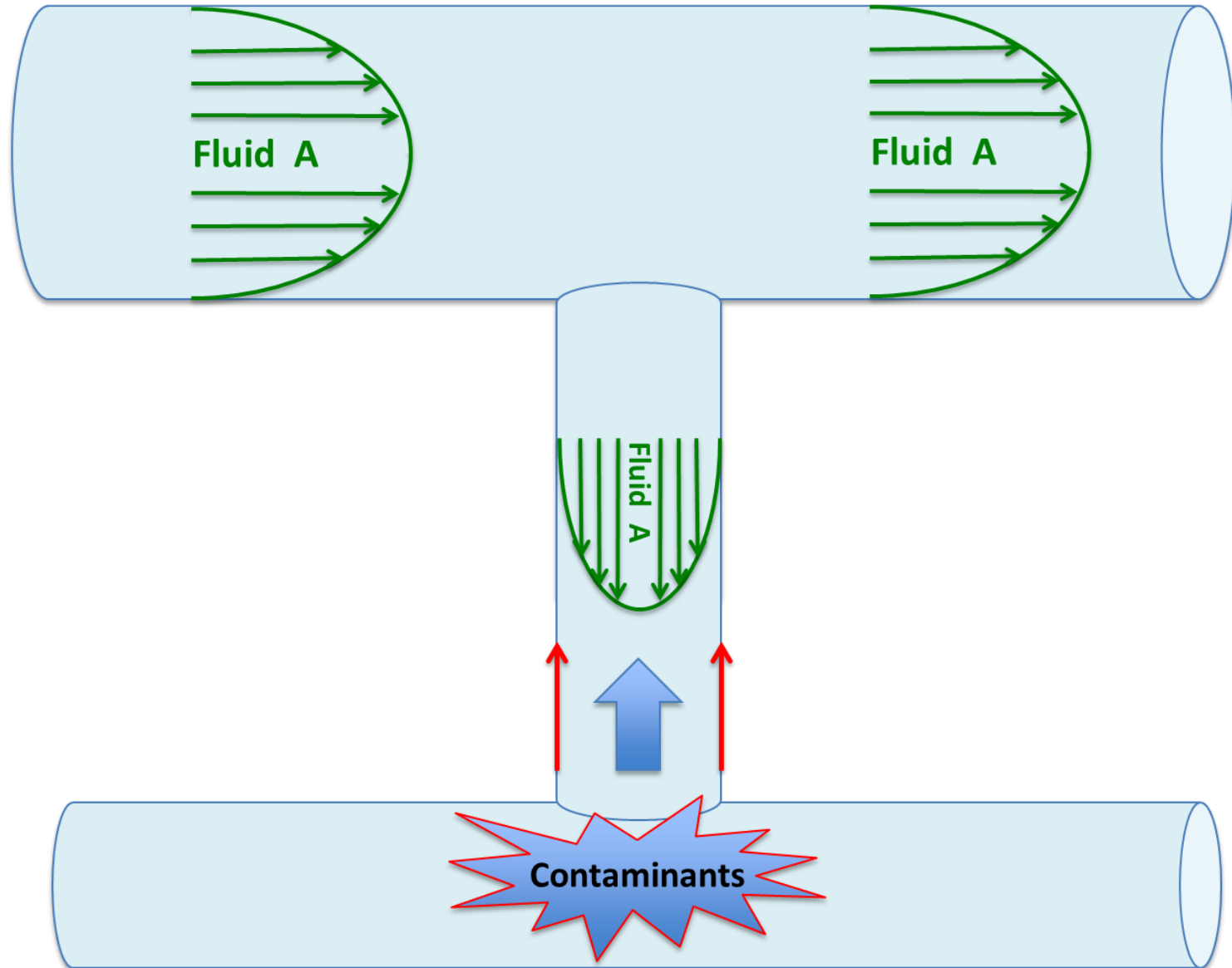
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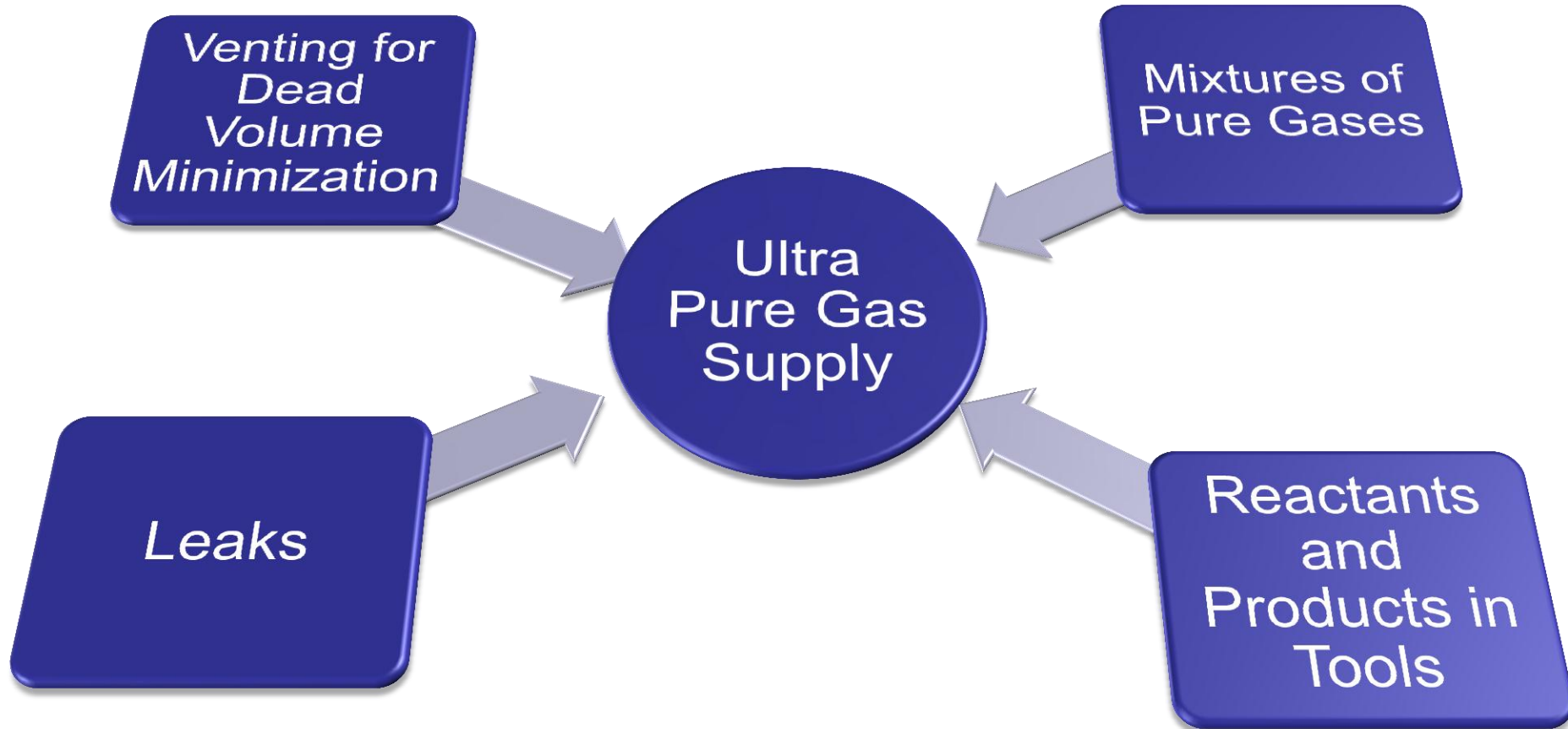
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Back Diffusion Sources and Mechanisms



Back Diffusion Sources and Mechanisms



Objectives

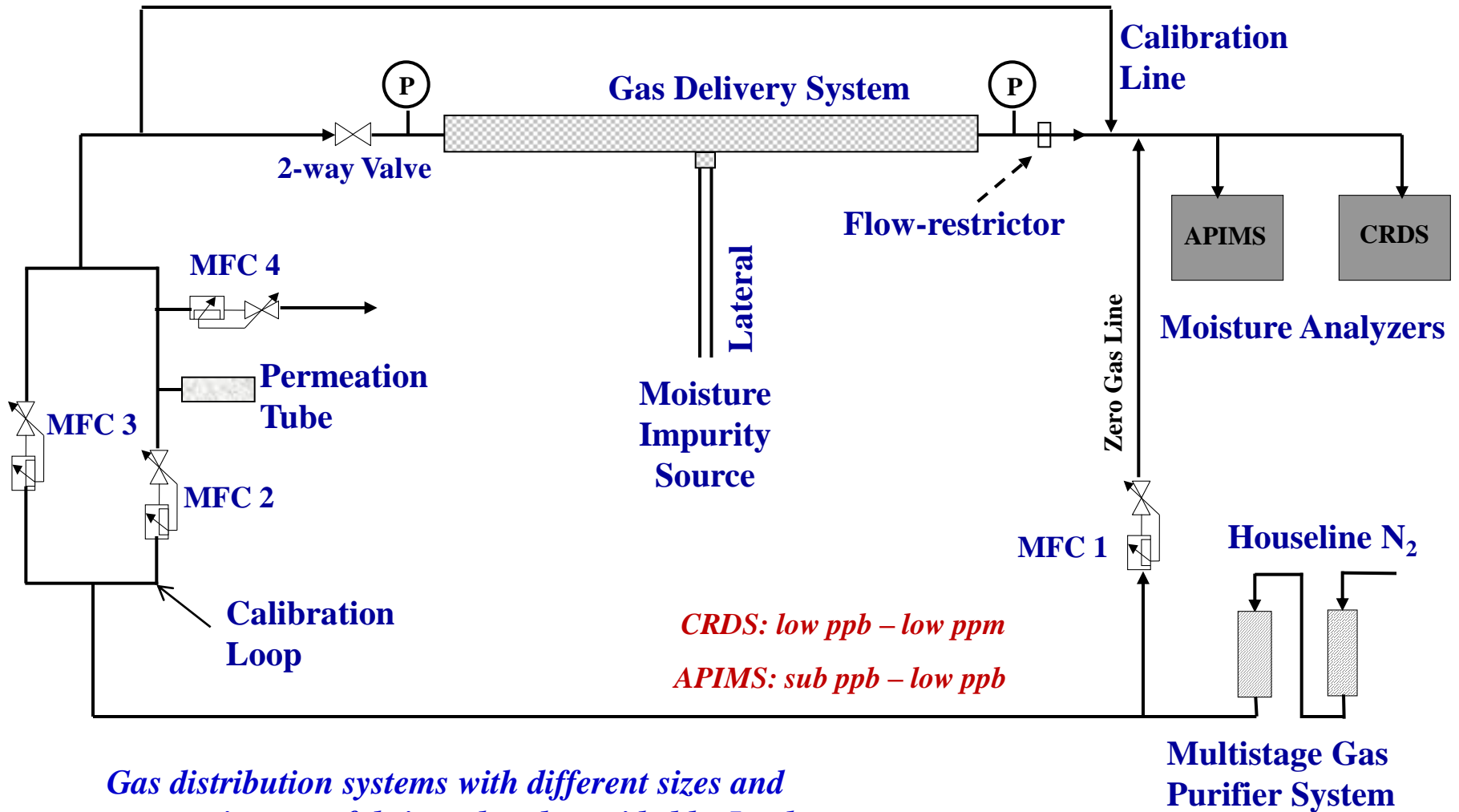
- **Developing operational parameters that will minimize back diffusion of impurities into fluidic distribution systems.**
- **Developing and validating a process simulator that can help industry design and operate systems while minimizing back diffusion, gas usage, and system dead volumes.**
- **Develop a better understanding of back diffusion since little is known or has been published on the subject.**

Motivation and ESH Impact

- **Contamination of gas distribution systems during normal operation results in major wasting of materials, energy, and valuable tool operation time.**

Experimental Testbed

Laterals Added to the Main Line



Gas distribution systems with different sizes and geometries were fabricated and provided by Intel

Back Diffusion Process Simulator

Convective Flux

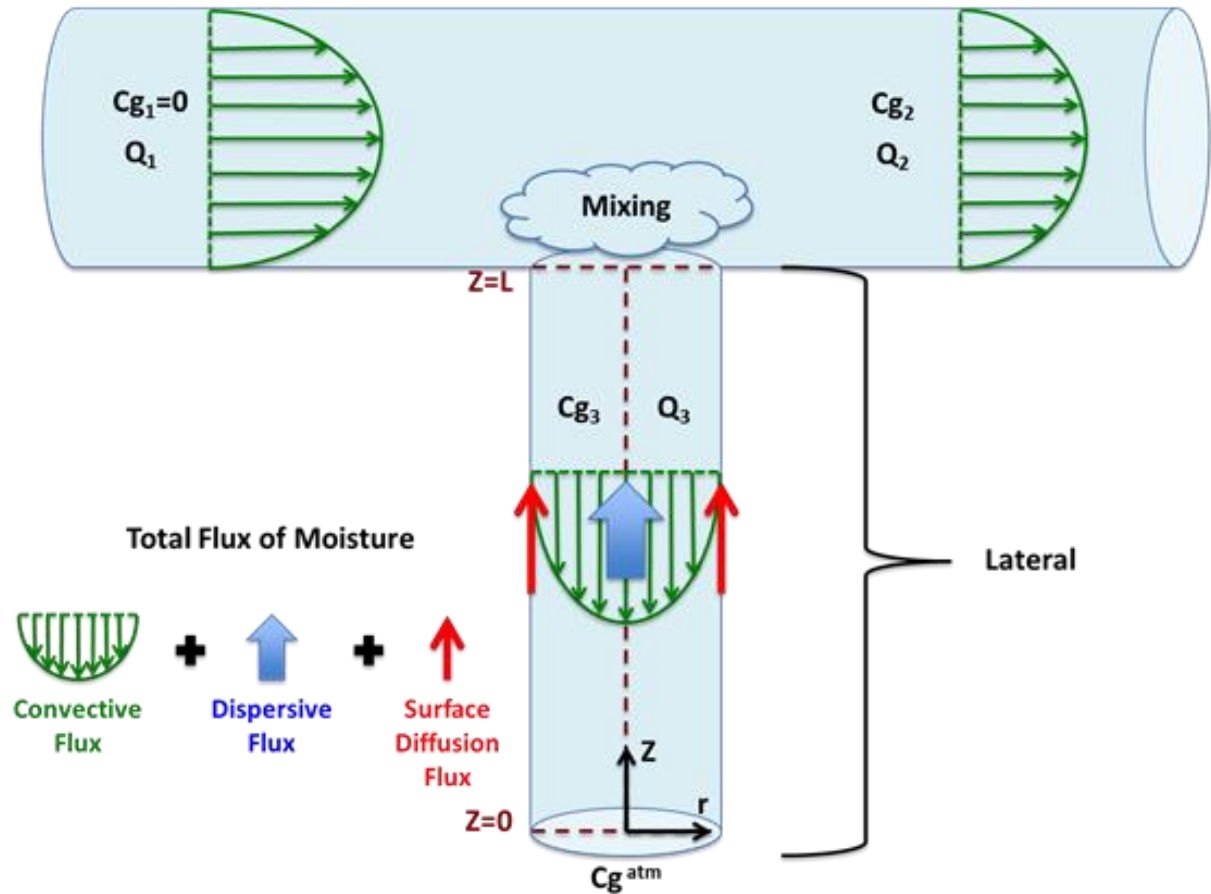
$$J_c = -U_3 C_g$$

Gas Phase Dispersive Flux

$$J = -D \frac{dC_g}{dz}$$

Surface Diffusive Flux

$$J_s = -D_s \frac{dC_s}{dz} - D_s \frac{k_a}{k_d} \frac{dC_g}{dz}$$



Total Dispersive Mass Flow Rate

$$\pi r^2 J_e = \pi r^2 J + 2\pi r J_s$$

Total Effective Dispersive Flux

$$J_e = -D_e \frac{dC_g}{dz}$$

Effective Dispersion Coefficient

$$D_e = D + \frac{2}{r} D_s K_e$$

Back Diffusion Process Simulator

Governing Equation

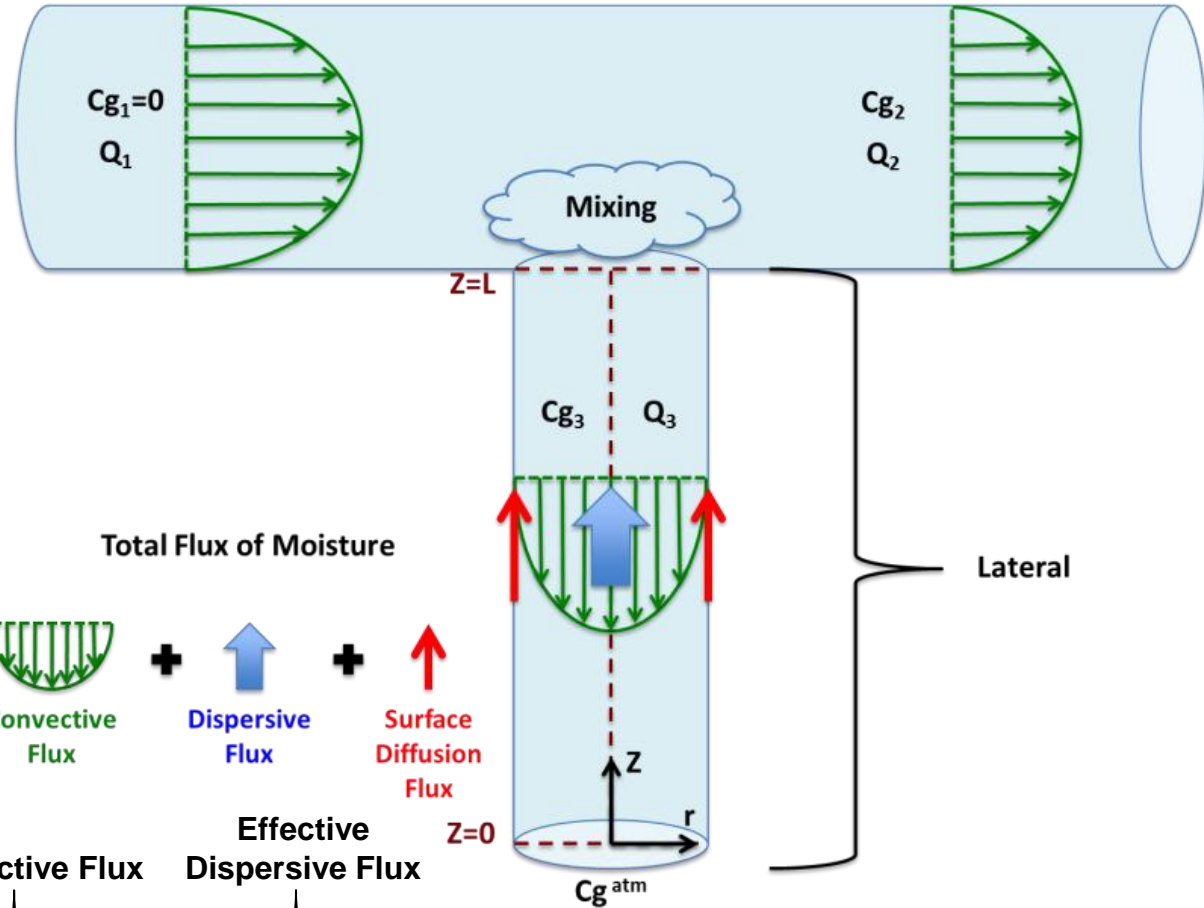
$$\underbrace{U_3 \frac{dC_g}{dz}}_{\text{Convection}} + \underbrace{D_e \frac{d^2 C_g}{dz^2}}_{\text{Effective Dispersion}} = 0$$

Boundary Condition 1

$$z = 0, \quad C_g = C_g^{atm}$$

Boundary Condition 2

$$z = L, \quad C_g \Big|_{z=L} = \left(\underbrace{-U_3 C_g \Big|_{z=L}}_{\text{Convective Flux}} - \underbrace{D_e \frac{dC_g}{dz} \Big|_{z=L}}_{\text{Effective Dispersive Flux}} \right) \frac{A_{lateral}}{Q_2}$$

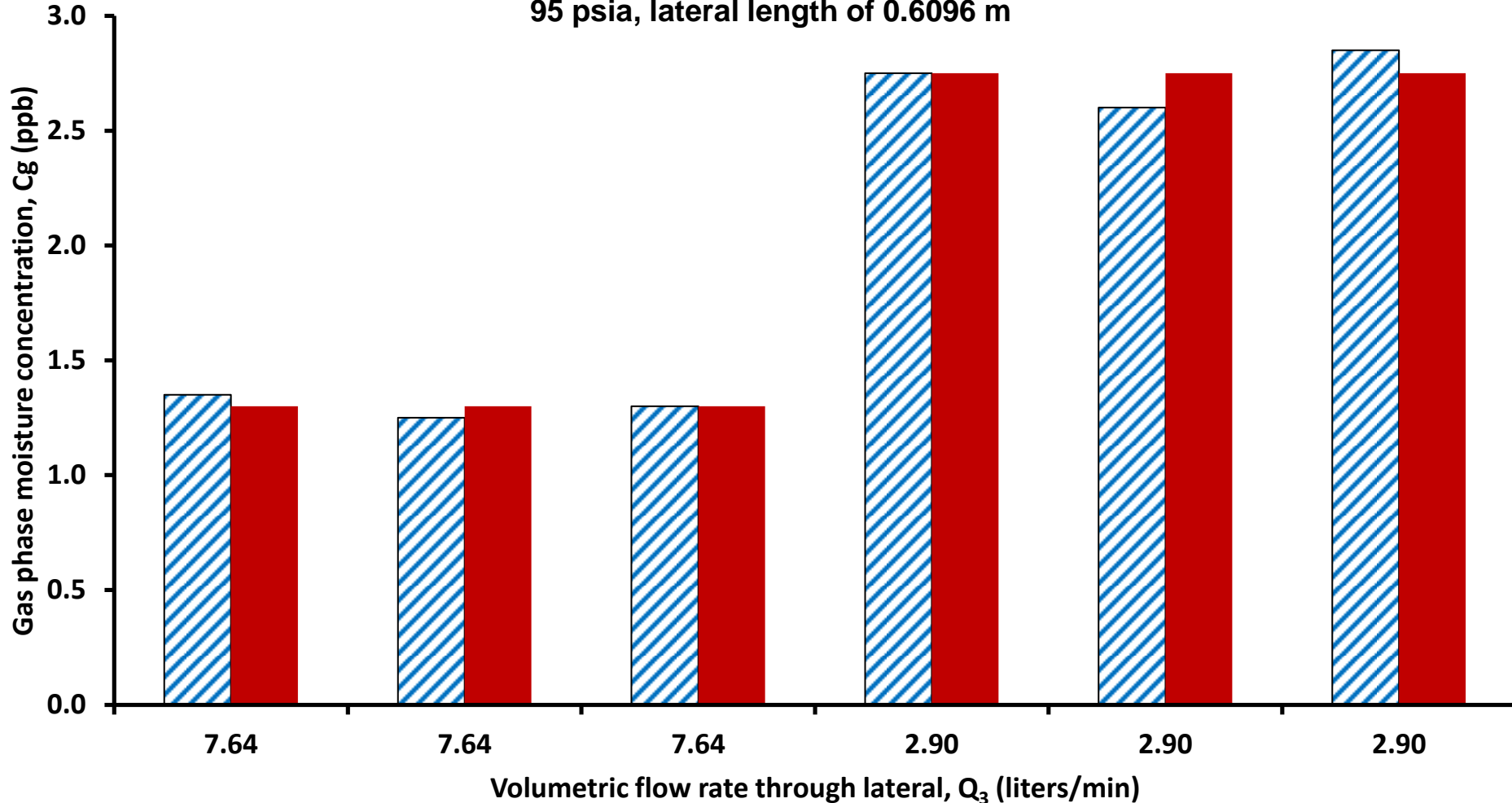


Process Simulator Verification

Simulator Prediction

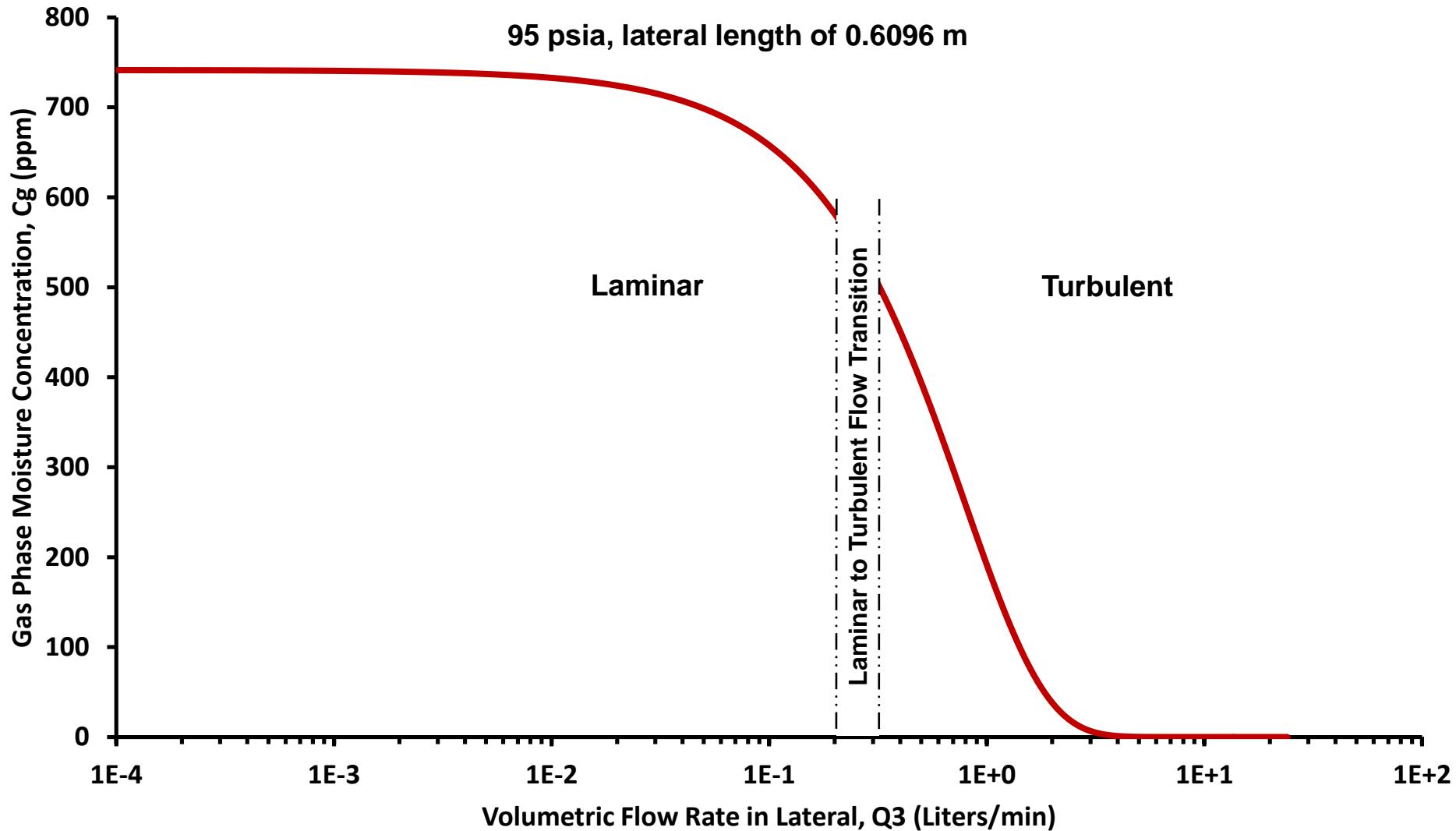
Experimental Results Model Prediction

95 psia, lateral length of 0.6096 m



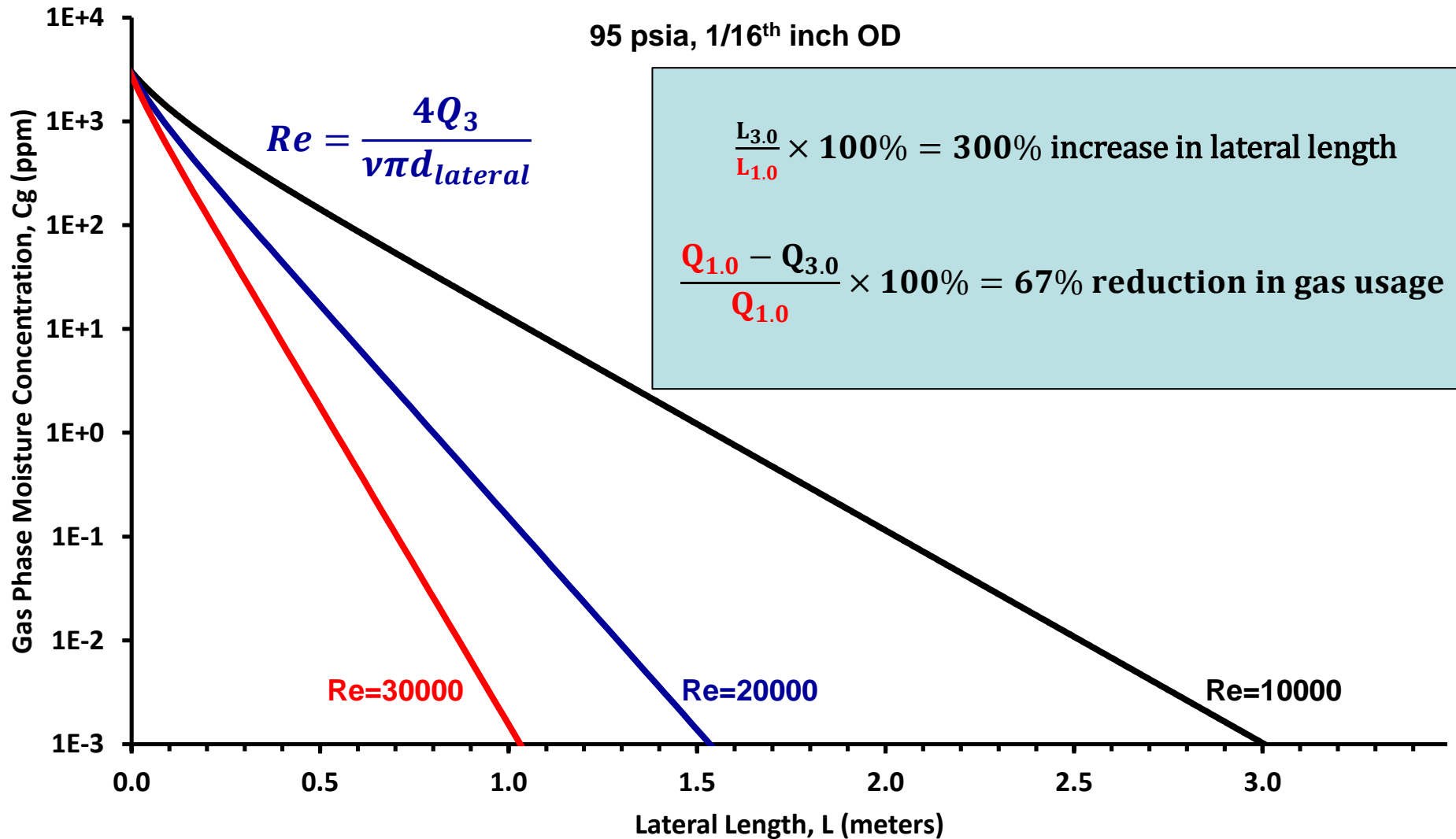
Parametric Studies

Effect of Flow Rate on Gas Phase Moisture



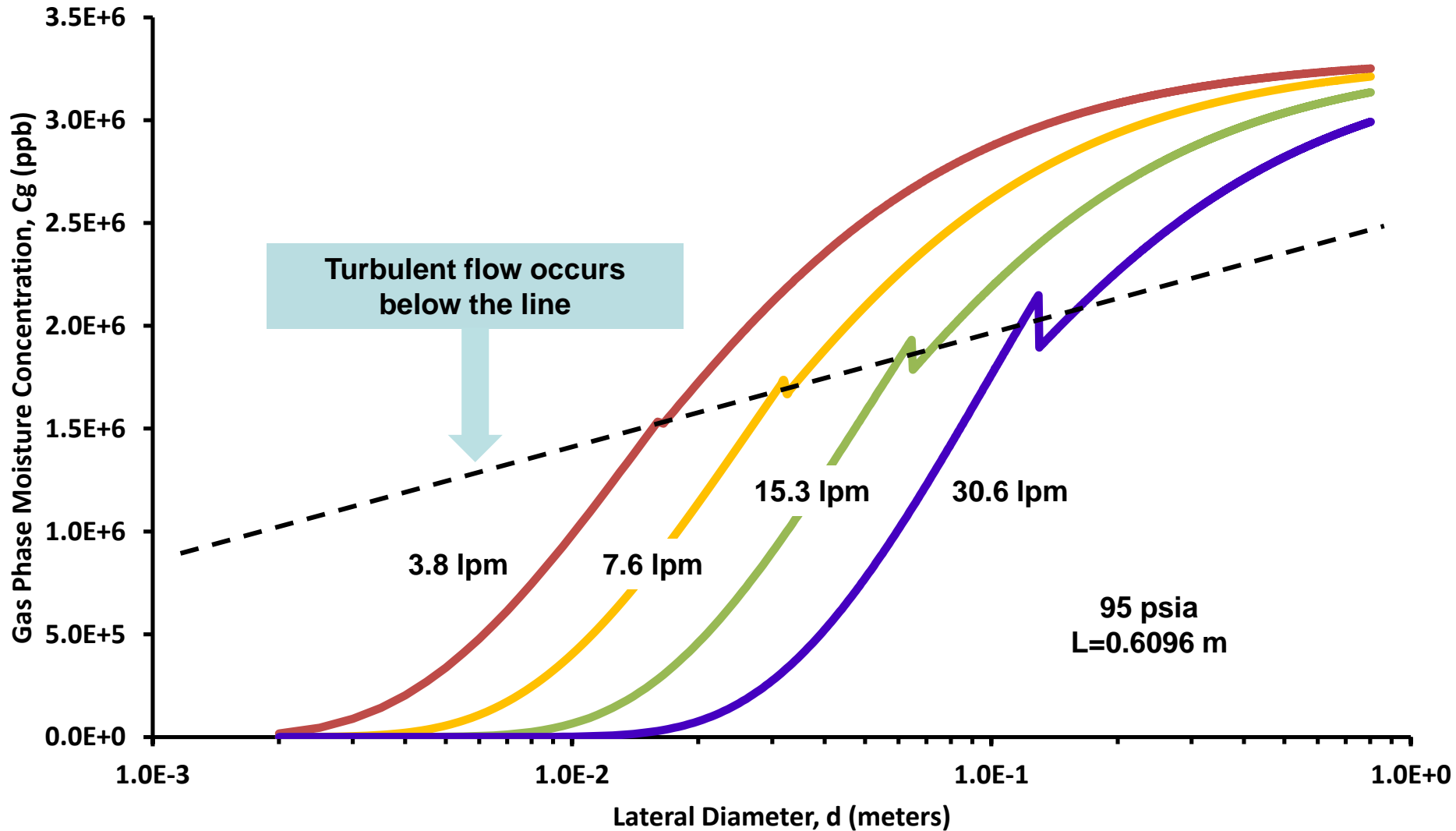
Parametric Studies

Effect of Lateral Length on Gas Phase Moisture



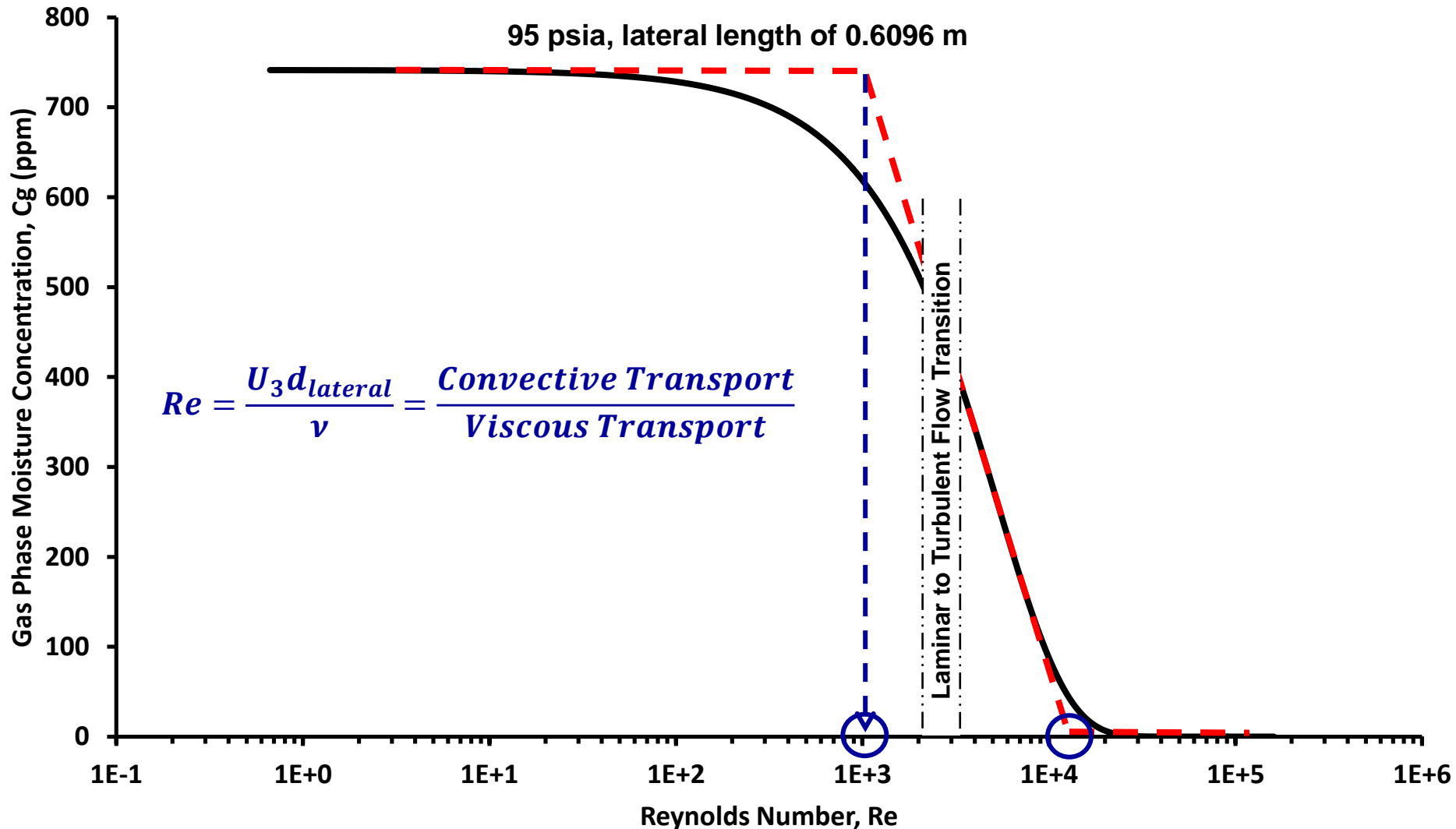
Parametric Studies

Effect of Lateral Diameter on Gas Phase Moisture



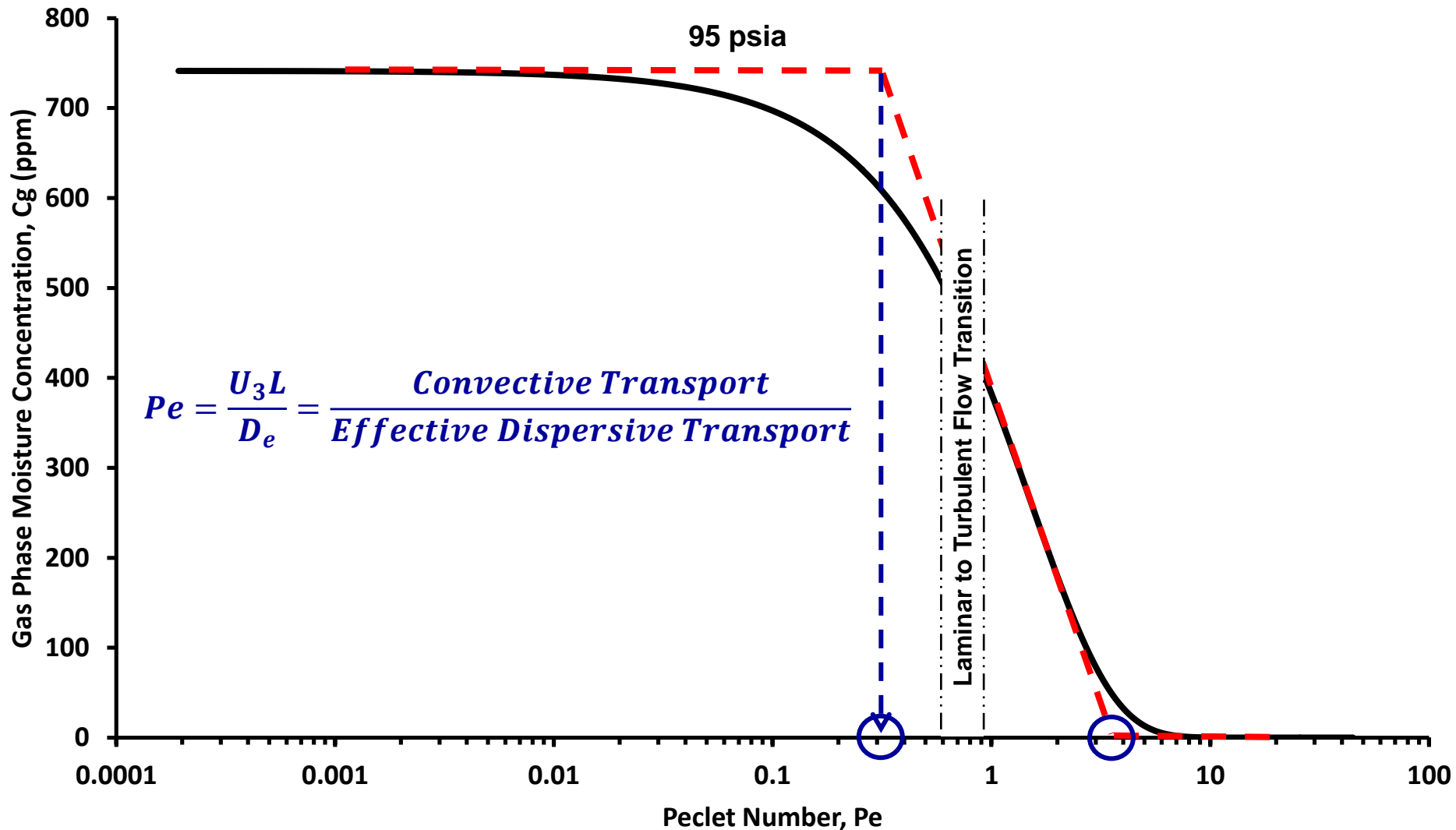
Parametric Studies

Effect of Reynolds Number on Gas Phase Moisture



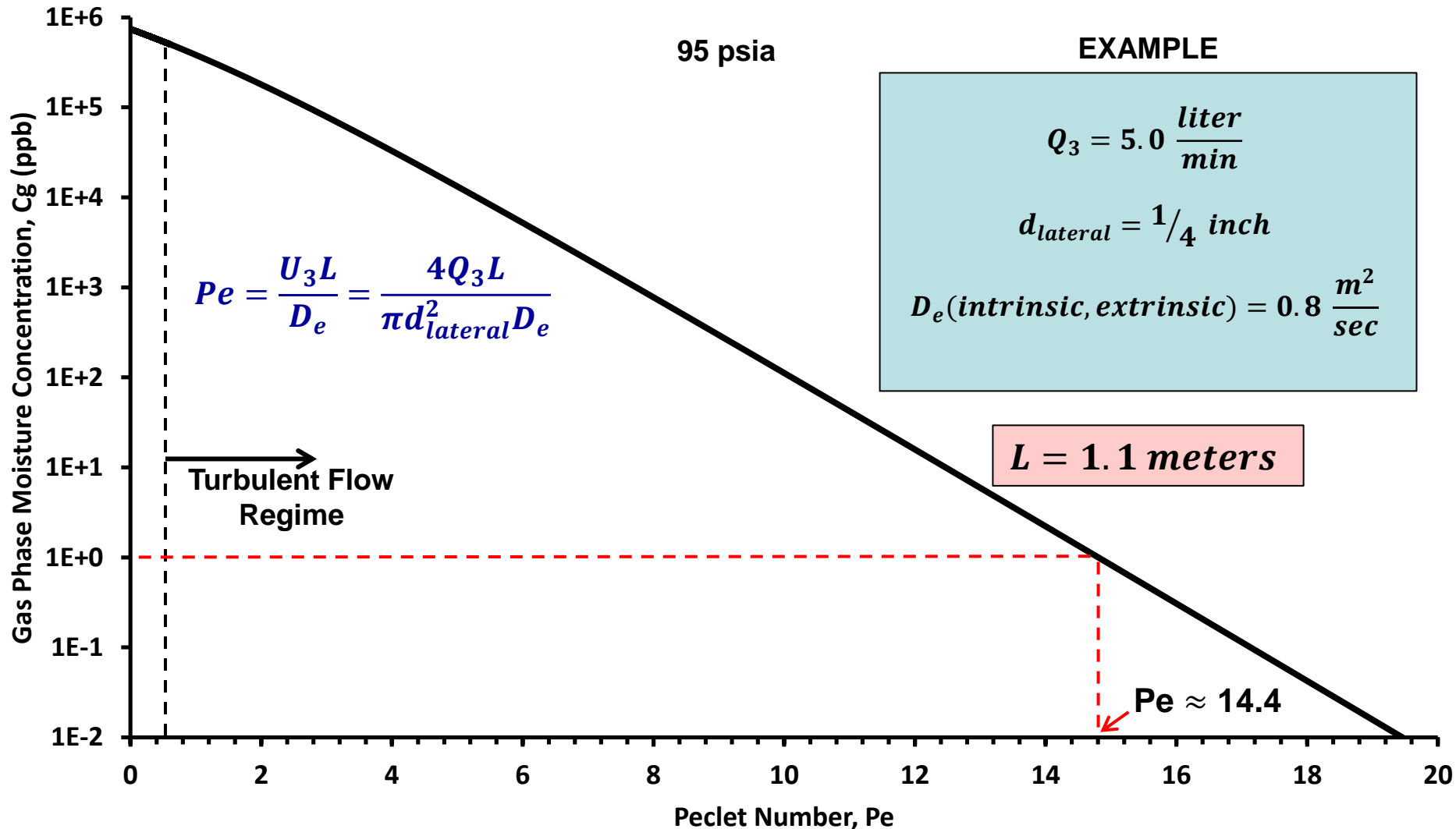
Parametric Studies

Effect of Peclet Number on Gas Phase Moisture



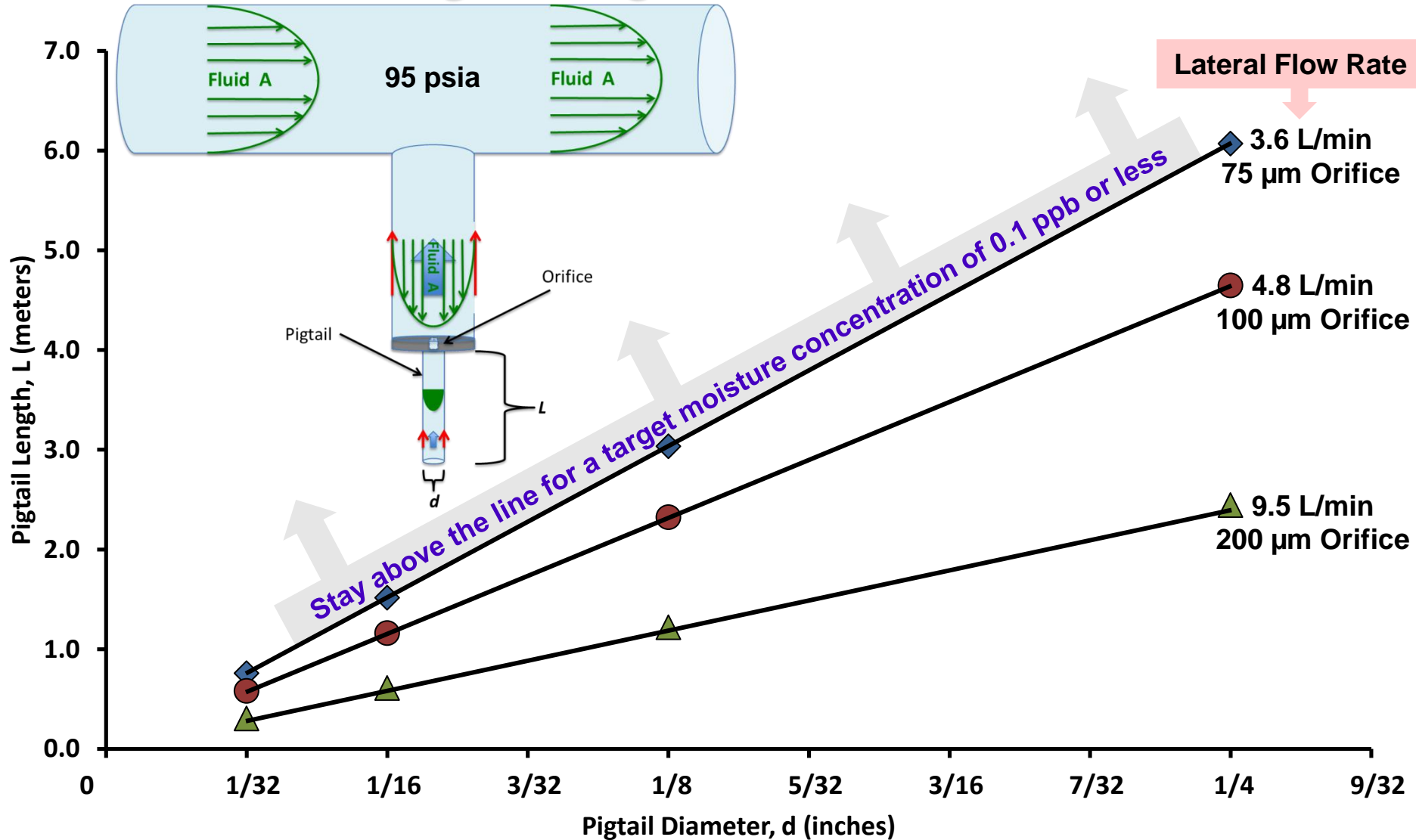
Parametric Studies

Effect of Peclet Number on Gas Phase Moisture



Parametric Studies

Pigtail Length and Diameters



Highlights

- **The experimental approach allowed for the observation of back diffusion in an adjustable and controllable manner.**
- **The process model accurately predicted experimental results and was invaluable in performing parametric studies.**
- **The moisture contamination due to back diffusion was a strong function of lateral diameter, length, and gas flow rate through the lateral.**
- **Characteristic groups were identified that allowed us present generalized correlations that would help in the design and operation of UHP fluidic systems being exposed to a source of contamination**
- **This methodology was expanded to include an orifice and pigtail in series and was effective in determining a design that will safeguard against the back diffusion of impurities into both bulk and process gases.**

Industrial Interactions and Future Plans

- **Continue our work with Intel on novel impurity control strategies to reduce gas usage**
- **Making the process simulator available to industry**
- **Extend the present study to other fluids, contaminants, and components**

Acknowledgements

- **Carl Geisert, Intel**
- **Tiger Optics support team**
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