

# **Novel Processes for Water Purification and Wastewater Treatment**

## **Catalytic Method for Water Purification**

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**Co-Sponsored by Pall Corporation**

# Purpose and Direction

## Objectives:

- Develop a novel environmentally benign water purification method

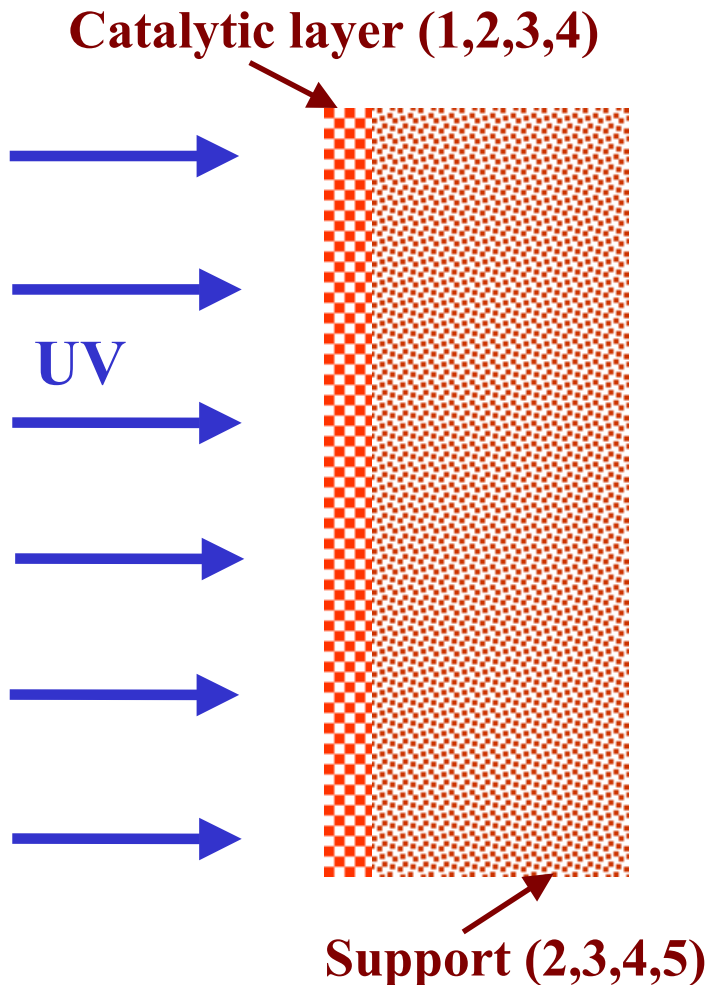
## ESH Impact:

- Low energy, low chemical usage, low waste
- Facilitating larger degree of water recycling

## Method of Approach:

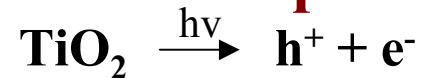
- Fundamental study of integrating catalysis with membrane filtration and/or degasification
- Experimental validation of the technology
- Work with supplier towards development of the first generation of this catalytic treatment

# Photo-Catalytic Activity

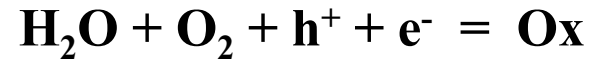


## Functions:

### 1. Electron-hole pair formation



### 2. Radical generation



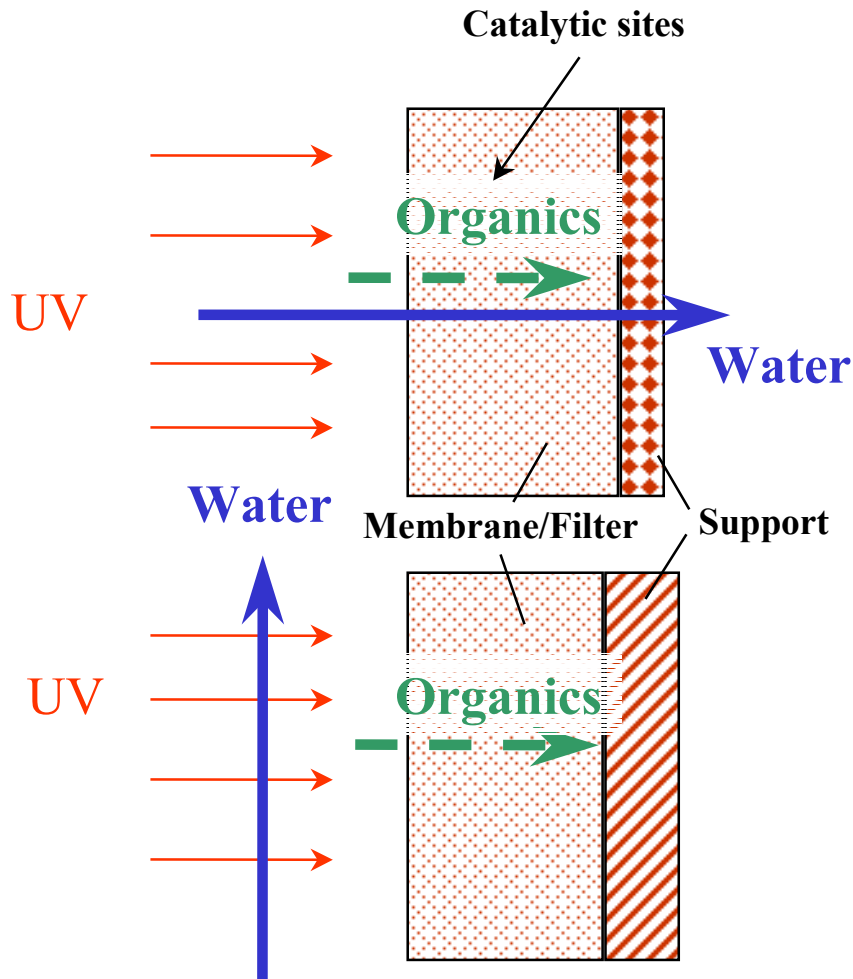
### 3. Impurity adsorption

### 4. Oxidation reaction



### 5. Radical quenching

# Two Photo-Catalytic Configurations



**Flow-through configuration:**

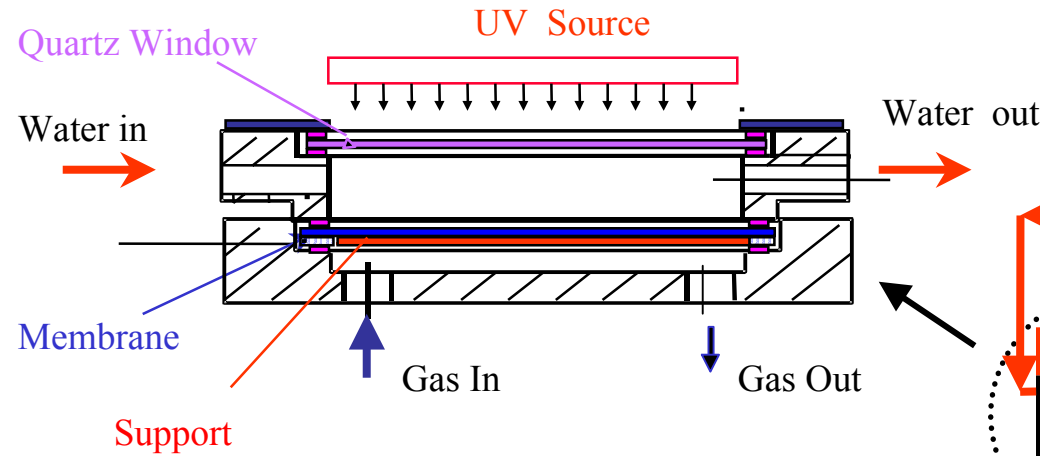
- Oxidation
- Depth filtration

**Tangential configuration:**

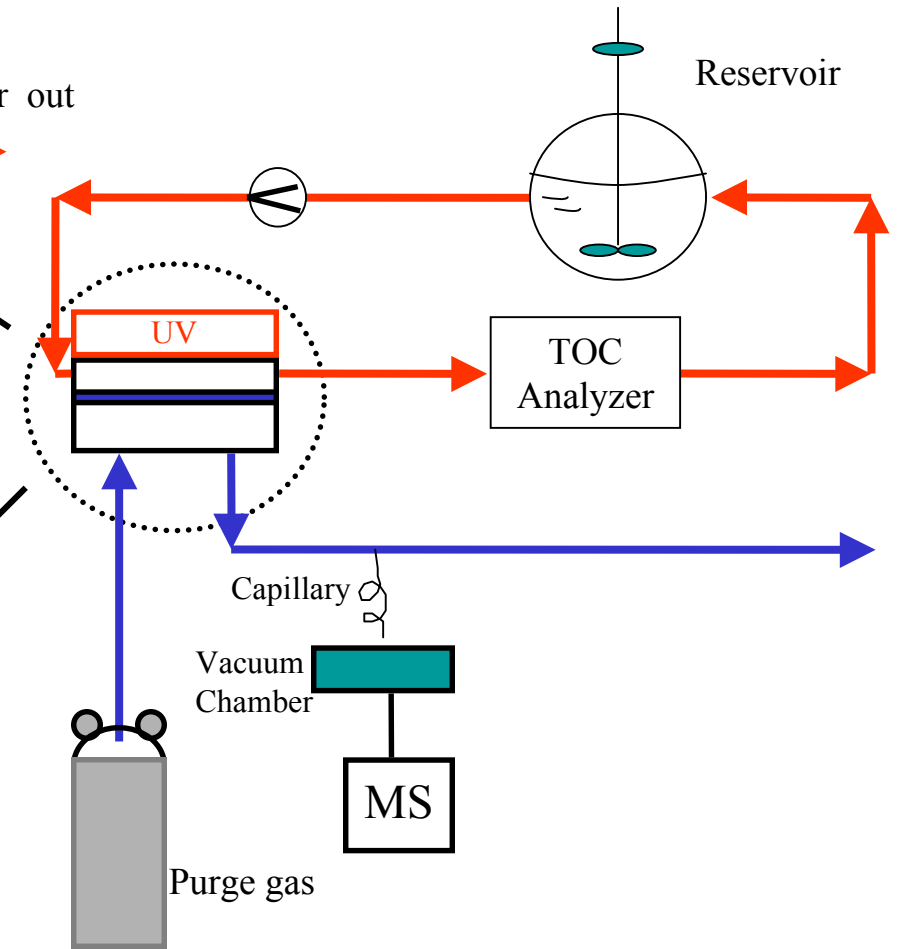
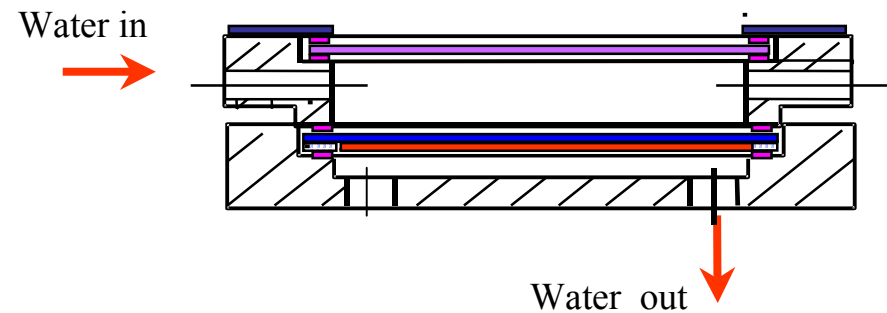
- Oxidation
- Degasification

# Experimental setup

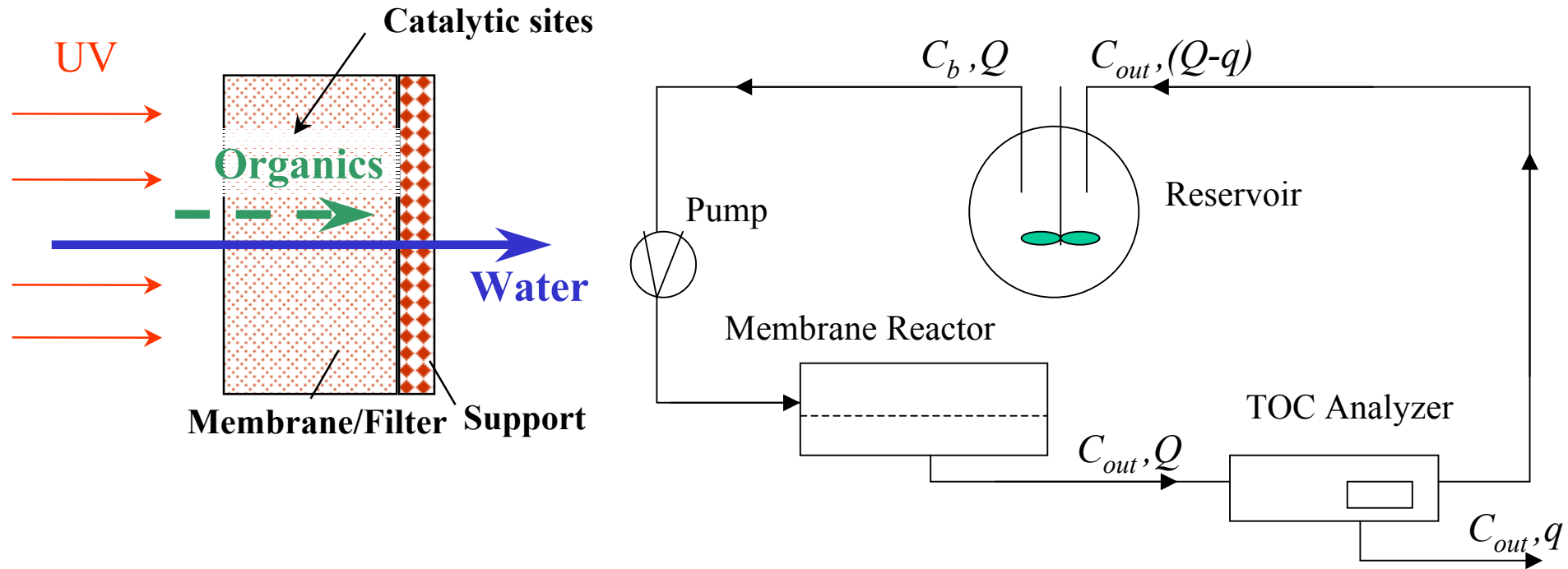
## Tangential flow configuration



## Flow-through configuration



# Flow-through Filtration



## Flow-through configuration:

- Oxidation
- Depth filtration

# Flow-through Filtration Process Model

- Characterization of diffusion and reaction within the catalytic membrane.

$$\frac{\partial C}{\partial t} = -v_x \frac{\partial C}{\partial x} + \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right) - kC$$

## *Simplifications:*

1. Pseudo-steady state

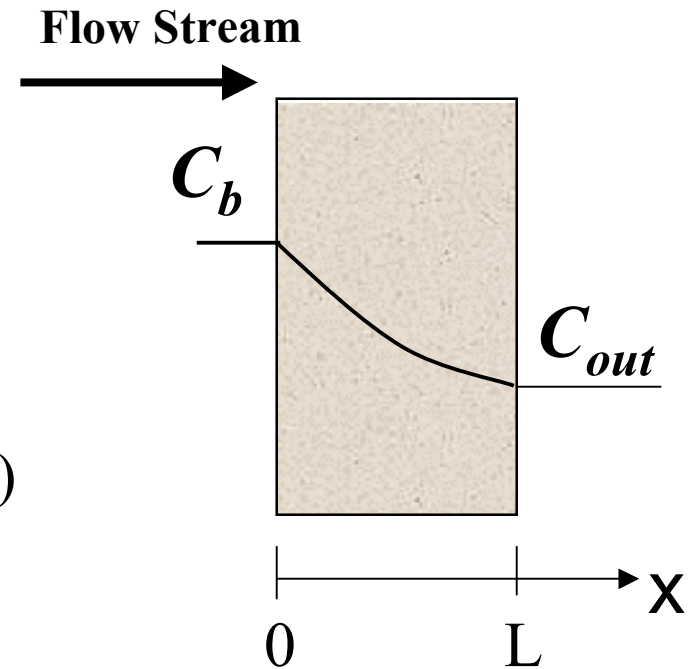
$$\frac{\partial C}{\partial t} = 0$$

2. Diffusion is negligible

$$v_x \frac{\partial C}{\partial x} \gg \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right)$$

3. Reaction rate coefficient is not a constant

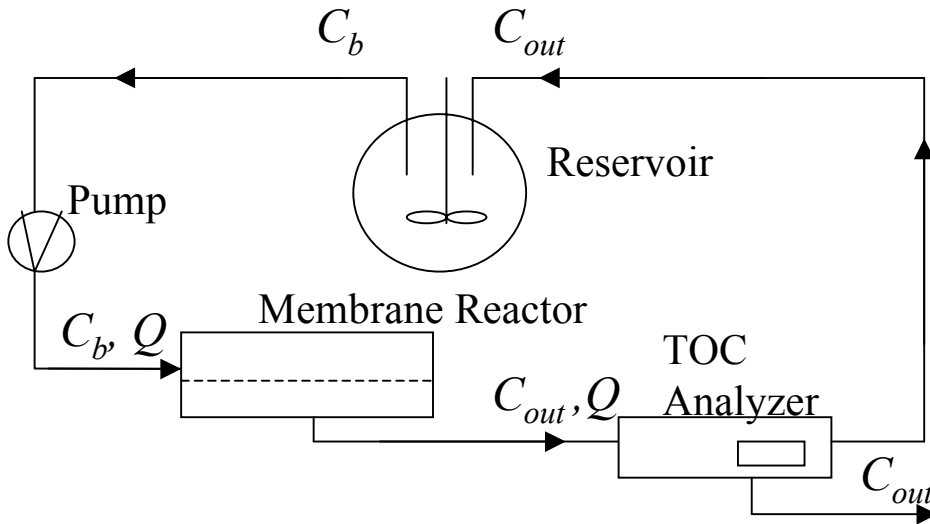
$$k = k_0 \exp(-\alpha x)$$



$$-v_x \frac{\partial C}{\partial x} = k_0 \exp(-\alpha x) C$$

# Flow-through Filtration Process Model

- **Characterization of time dependent interaction between membrane reactor and reservoir.**



## *Simplifying Assumptions:*

1. Membrane reactor is CSTR
2. Reservoir is CSTR
3. No mixing along the tubing
4. Waste stream out of TOC analyzer is neglected

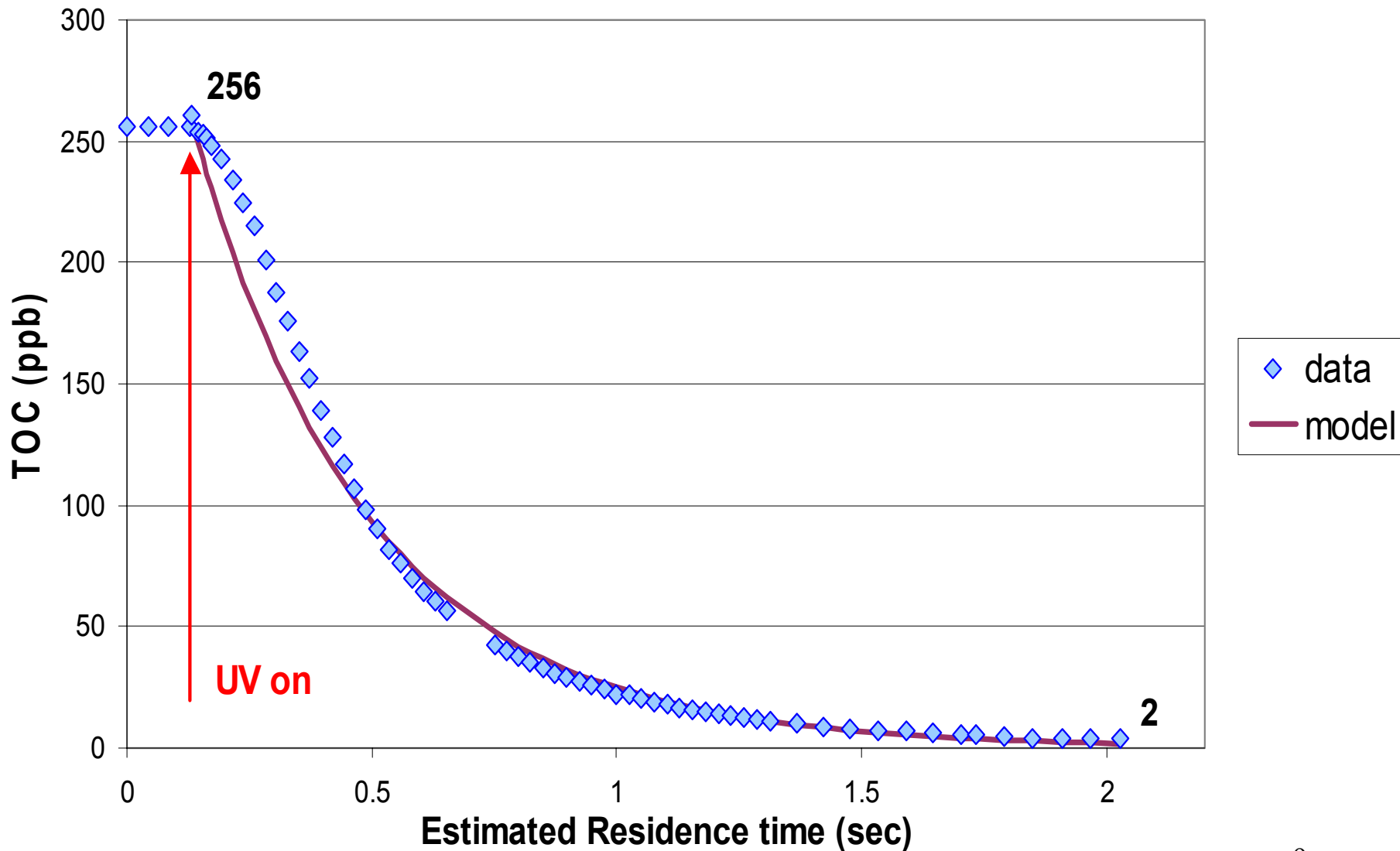
$$C_{out}(t) = C_{initial} \exp\left[\frac{Q(A-1)}{V_{reservoir}} \times t\right] \times A,$$

where

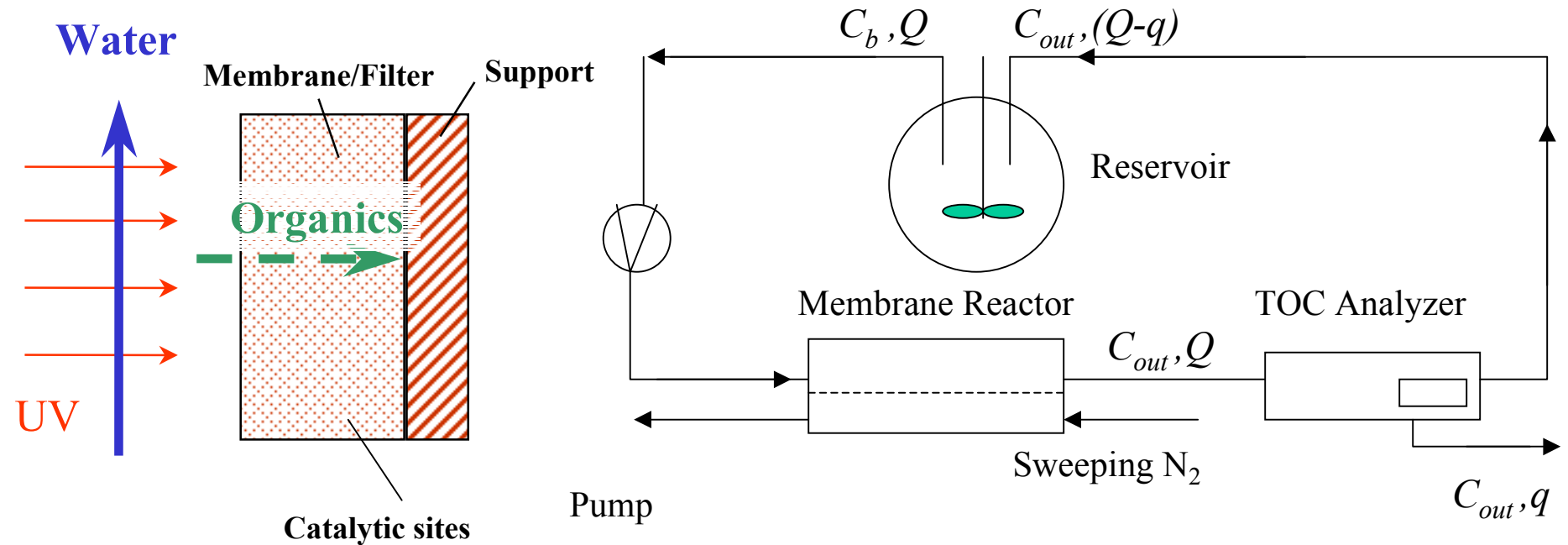
$$A = \exp\left[\frac{-k_0}{v \times \alpha} (1 - \exp(-\alpha L))\right]$$



# Flow-through Filtration, Model and Experimental Comparison



# Tangential Flow Degasification



**Tangential configuration:**

- Oxidation
- Degasification

# Tangential Flow Degasification Process Model

- Characterization of transport and reaction in four zones.

## I. Interphase Transport

$$J = km(C_b - C_s)$$

## II. Equilibrium at the Interphase

$$K_e = \frac{C_1}{C_s}$$

## III. Diffusion and Reaction

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right) - kC$$

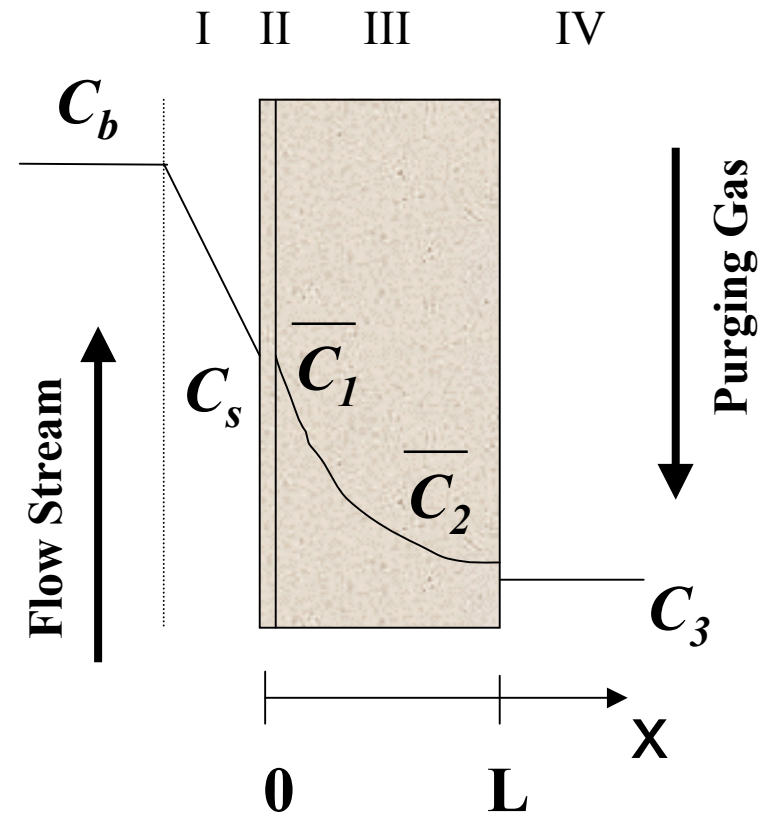
*Assumptions:*

1. Pseudo-steady state
2. Reaction rate coefficient is constant
3. Diffusion coefficient is constant

$$D \left( \frac{\partial^2 C}{\partial x^2} \right) = kC$$

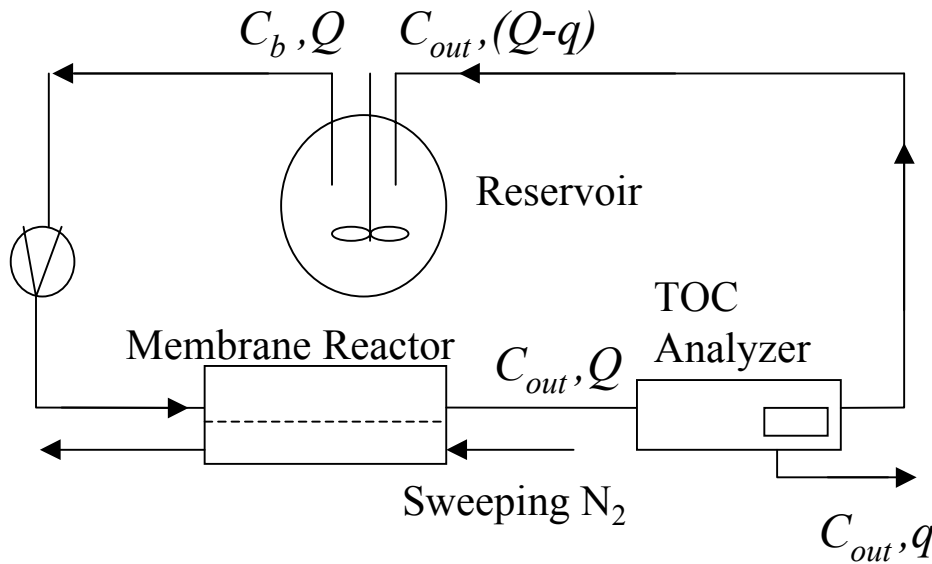
## IV. Desorption

$$K_d = \frac{C_2}{C_3}$$



# Tangential Flow Degasification Process Model

- Characterization of time dependent interaction between membrane reactor and reservoir.



## *Assumptions:*

1. Membrane reactor is CSTR
2. Reservoir is CSTR
3. No mixing along the tubing

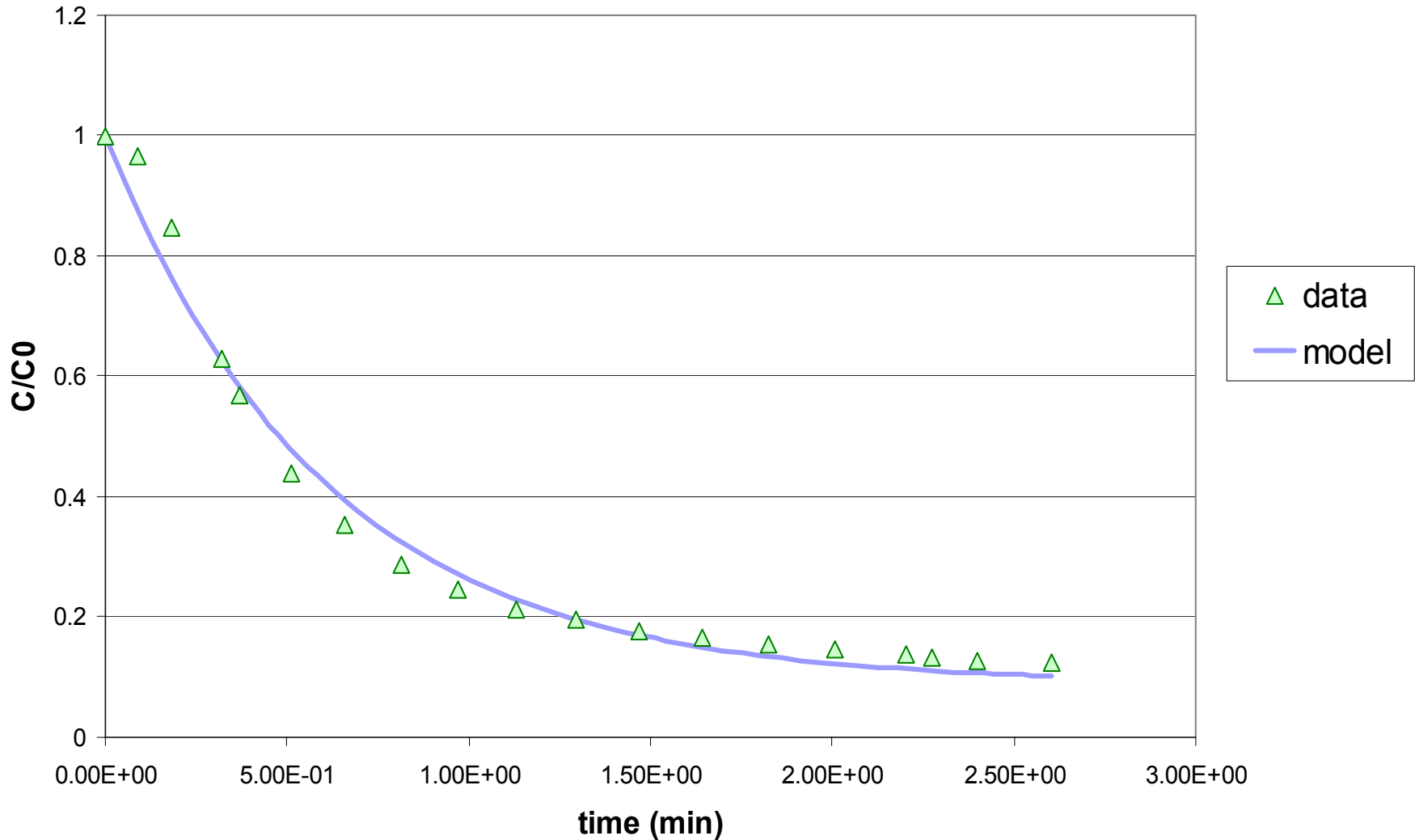
### Mass Balance Equation for reservoir:

$$\frac{dC_{in}}{dt} \times (V_{reservoir} - qt) = C_{out} \times (Q - q) - C_{in} \times Q \quad ,$$

### Mass Balance Equation for reactor:

$$\frac{dC_{out}}{dt} \times V_{reactor} = C_{in} \times Q - C_{out} \times Q - J \times S$$

# Tangential Flow Degasification, Model and Experimental Comparison



# Conclusions

- **Photo-Catalytic membranes have been proven to be effective for removal of organic contaminants**
- **A hydrophobic membrane incorporating the ERC catalytic technology has been synthesized and tested (jointly with Pall Corporation)**
- **Process models have been developed and shown to be useful for estimating process parameters for both tangential and flow-through configurations.**

# Acknowledgements

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