

# Manufacturing Qualification of an All Dry De-veil Plasma Process

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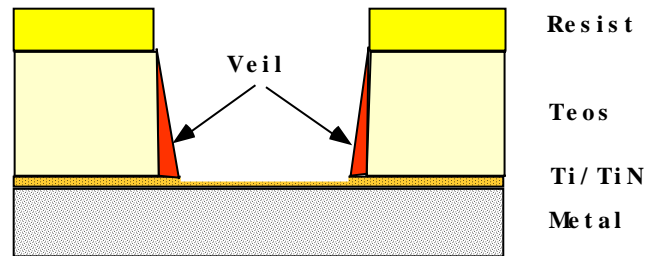
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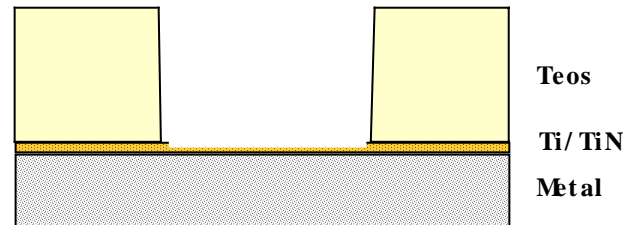
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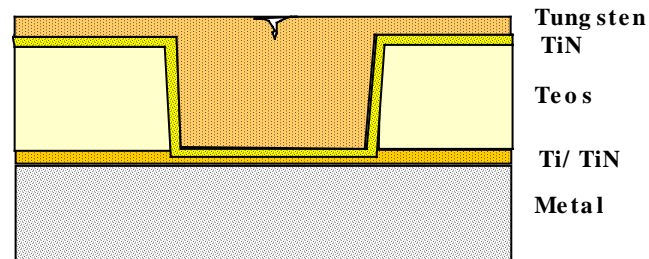
# Via Process Integration



**Post Via Etch**



**Post Ash/Deveil**



**Via Metal Fill**

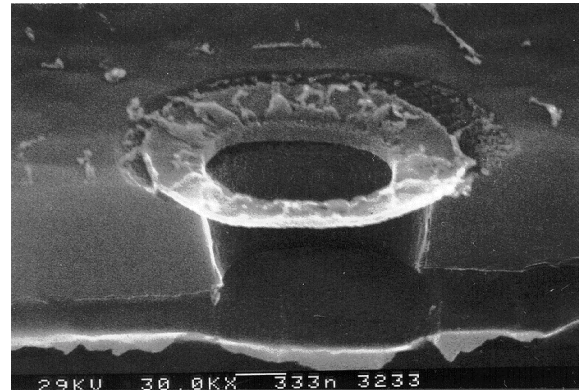
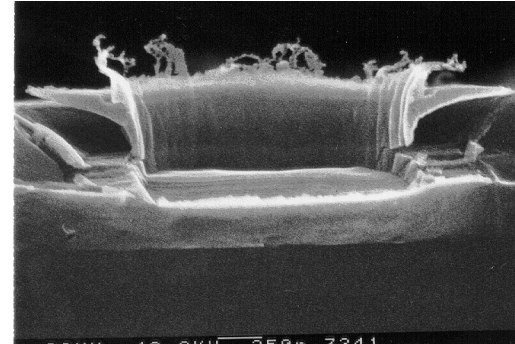
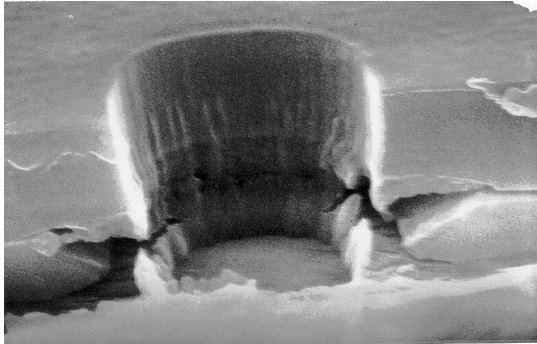


# Problem Statement

- Via veil, or metallized polymer, is an unwanted by-product of via etch. Traditionally, these veils are removed with organic or inorganic solvents. Inorganic solvents, while effectively dissolving veils under ideal conditions, are costly and inconsistent under non-ideal conditions. Solvents are also environmentally incompatible. For these reasons, a dry solution has been explored.

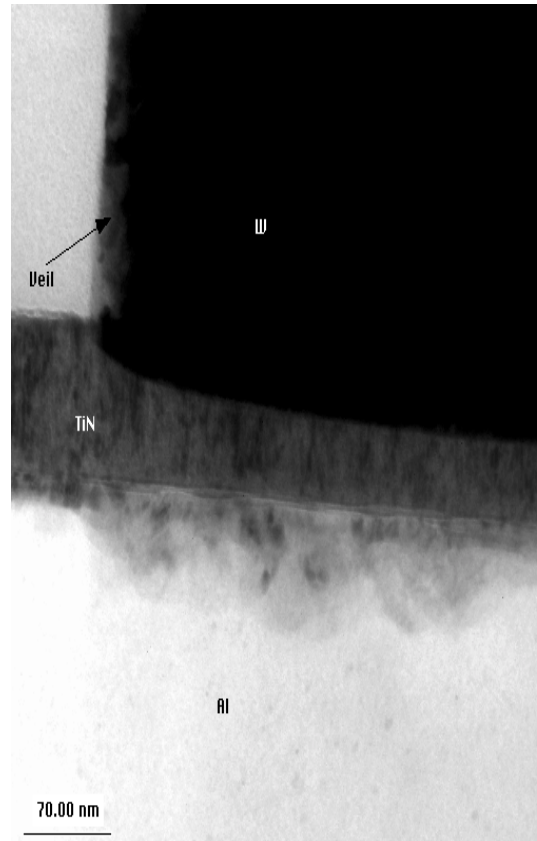


# The Problem: Via Veils



\* veils produced using stop-on-Al via test structures

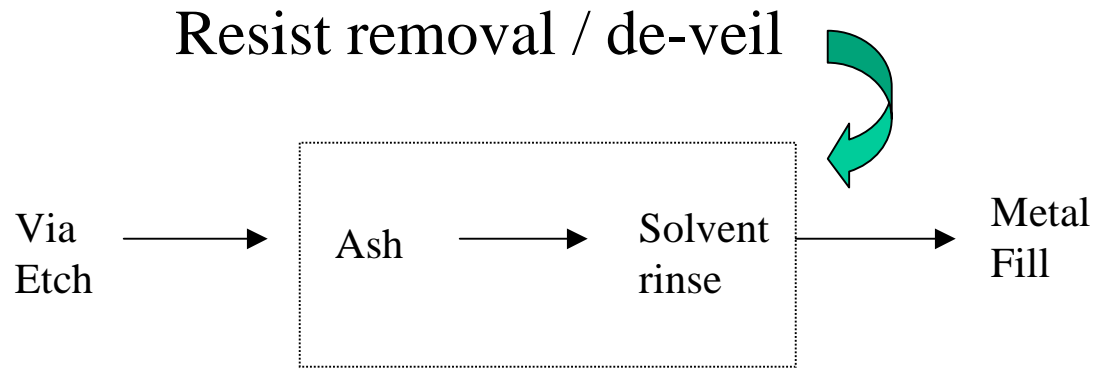
# Via Veil: Stop-on-TiN Via



\* ash only processing  
no de-veil.



# Solvent De-veil Process



1. O<sub>2</sub>/N<sub>2</sub> ash to remove resist. >240 °C process temp

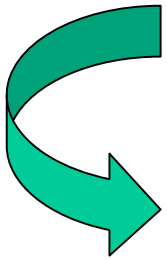
2. Hydroxyl amine (HA) solvent de-veil done in hood or spray tool.

Spray Process: HA (80 °C) rinse followed by isopropyl alcohol and DI water rinse.



# Solvent De-veil Process, cont'd

- HA chemical effectiveness dependent on temperature and water concentration.
- Spray tools are difficult to control and to monitor. Hoods require large floor space.
- Aggressive nature of HA tends to pit AlCu and degrade valves and seals.
- Chemicals, chemical facilities, and chemical management are costly and relatively unfriendly to the environment.



These difficulties lead to product variation, scrap, high cost and environmental burden.

# Solvent Spray Tool





# Solvent Handling Facilities



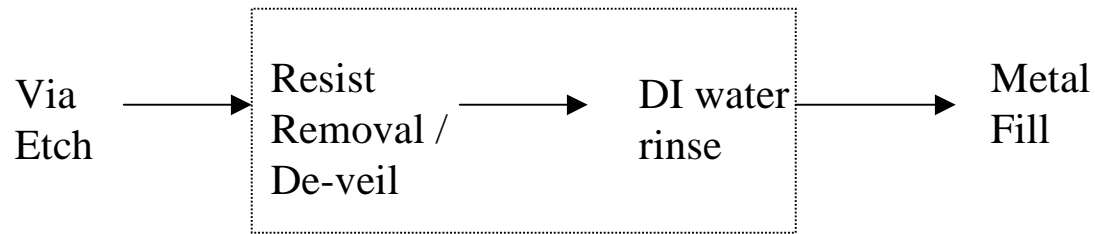
\* 5700 gal chemical reclaim tanks

# Dry De-Veil Theory

- The addition of free fluorine to the  $O_2/N_2$  Ash chemistry at reduced temperature will make the veil more soluble, thus more readily removed with DI water only. This is based on the fact that  $Al_2F_3$  is more soluble than  $Al_2O_3$ .



# Dry De-Veil Process



- 1. Resist removal and veil treatment using  $\text{NF}_3/\text{O}_2$  plasma process at 25-90 °C.**
- 2. Room temperature DI water rinse.**



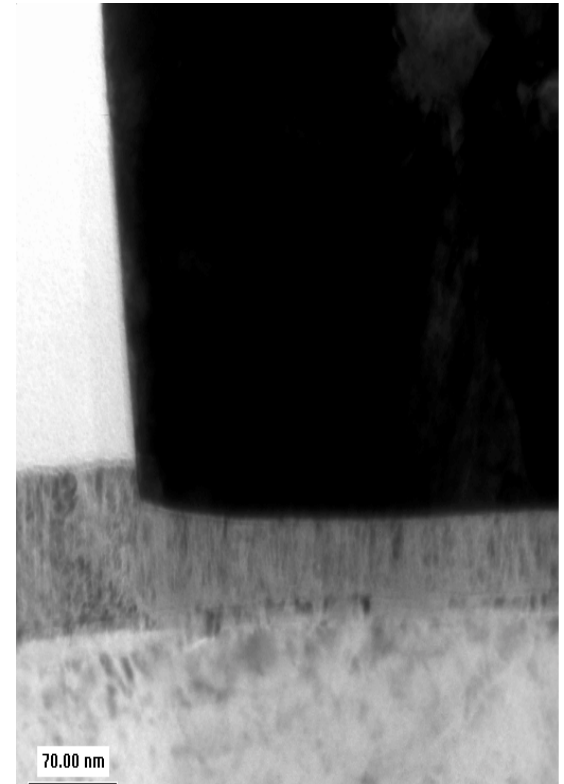
# Dry De-Veil Process, cont'd

- Dual process steps: bulk resist removal and veil treatment
- Chemistry:  $\text{NF}_3$  or  $\text{CF}_4$ ,  $\text{O}_2$ ,  $\text{N}_2$  or  $\text{H}_2\text{N}_2$  (forming gas, 2%  $\text{H}_2$ )
- Dual power sources:
  - Downstream microwave: 0-2000W
  - RF for reactive ion etch: 0-650W
- Low temperature processing: 25-90 °C
- Optical Endpoint



# Dry De-Veil Results

- Product yield and resistance data is equivalent or better than solvent process
- Metal fill glue deposition is more uniform
- Solvent failure mechanisms have been eliminated.
- Product has been running with the new process since Q4'99.



# Dry De-Veil Process Tools



\* Dry de-veil tools and DI water Spin/Rinse/Dry tool



# De-veil Cost Comparison:

Assume: 10K wafer starts/wk, Triple layer metal (2 via layers)

<i>Cost Item</i>	<i>Solvent Process</i>	<i>Dry De-veil Process</i>
HA Solvent Cost	\$2,080,728 (41,614 gallons)	\$0
Isopropyl alcohol	\$2,741,566 (312,109 gallons)	\$0
DI Water	\$4,498 (391,134 gallons)	\$3,632 (315,900 gallons)
Process gas	\$8,786	\$98,758
Process power	\$969 (11,847 KWH)	\$765 (9,359 KWH)
Waste disposal	\$17,153	\$0
<b>TOTAL PROCESS COST</b>	<b>\$4,853,700</b>	<b>\$103,155</b>
<b>TOTAL PROCESS COST/WAFER PASS</b>	<b>\$4.66</b>	<b>\$0.10</b>
<b>TOTAL PROCESS COST/WAFER</b>	<b>\$9.33</b>	<b>\$0.20</b>

# Cost Comparison, cont'd

	<i>Solvent Process</i>	<i>Dry De-veil Process</i>
Equipment list	5 Spray Solvent Tools 4 Dry Ashers	7 Dry De-veil Tools 2 Spin Rinse Dryers
Annual amortization 5 yr. depreciation	\$860,664	\$802,800
Idling power costs	\$10,000	\$15,085
Annual component replacements	\$400,000	\$91,000
Tool set floor space requirement	243 sq ft	117 sq ft
TOTAL ANNUAL OVERHEAD COST	\$1,270,664	\$908,885
ANNUAL OVERHEAD COST/WAFER PASS	\$1.22	\$0.87
OVERHEAD COST/WAFER	<b>\$2.44</b>	<b>\$1.74</b>
PROCESS COST/WAFER	<b>\$9.33</b>	<b>\$0.20</b>
TOTAL ANNUAL COST/WAFER	<b>\$11.77</b>	<b>\$1.94</b>

Net Annual Savings at 10,000 wsw: \$5,111,600



# NF<sub>3</sub> Emission Analysis

1. Gases employed to process 520,000 product wafers<sup>1</sup> (2 passes/wafer)

O<sub>2</sub>: 1,074,320 liters

NF<sub>3</sub>: 57,200 liters

H<sub>2</sub>N<sub>2</sub>: 44,720 liters

2. Approximate raw exhaust gas composition during process, by volume<sup>2</sup>:

NF<sub>3</sub>: 1.3%                      CO<sub>2</sub>: 0.4%

HF: 0.2%                        CO: 0.8%

COF<sub>2</sub>: 0.7%                    O<sub>2</sub>: 96.6%

3. Using a GWP(Global Warming Potential) of 8,000 for NF<sub>3</sub><sup>3</sup>

Estimated MMTCE (million metric tons carbon equivalent) from NF<sub>3</sub>:

**7.5E-5**

Based on 52 wafer fabs<sup>4</sup>, MMTC from NF<sub>3</sub>: 3.9E-3

(The Semiconductor Industry generated approx. 1.4 MMTCE in 1996<sup>5</sup>)

1. Assuming a 10,000 wafer start/wk fab.

2. RGA data taken on production equipment with representative process.

3. Source: US EPA, Scott Bartos, SSA Annual Meeting, 2000.

4. Assuming 27 million wafers produced in 2000. Source: Rose Associates

5. Source: S. Karecki L. Pruette, R. Chatterjee, R. Reif, *Alternative Chemistries for Dielectric Etch Processes*, 1999.

# Process Qualification Normalized Device Yield Results

<b>Process</b>	<b>Yield</b>	<b>Standard Deviation</b>	<b>Number of Lots</b>
<b>Solvent Clean</b>	1.0	11.56	481
<b>Dry Deveil</b>	0.998	13.39	170



# Process Qualification

## 168 Hour Reliability Yield Results

<b>Split</b>	<b>168 Hour Burn-in Failures</b>
Control	0/197
Ulvac	0/197
Control	0/80
Ulvac	0/80
Control	0/100
Ulvac	0/84

PART	TOOL	LAYER	N LOTS	%KLVN FAIL	%CHAIN FAIL	QBD SHIFT
A	Solvent	Via 1	25	--	0.144	NO
	Dry	Via 1	19	--	0.030	
	Solvent	Via 2	25	--	0.018	NO
	Dry	Via 2	19	--	0.000	
C	Solvent	Via 1	25	0.027	0.000	NO
	Dry	Via 1	19	0.000	0.000	
	Solvent	Via 2	25	0.027	0.027	NO
	Dry	Via 2	19	0.000	0.000	
D	Solvent	Via 1	24	0.058	0.019	NO
	Dry	Via 1	13	0.000	0.000	
	Solvent	Via 2	22	0.042	0.021	NO
	Dry	Via 2	9	0.000	0.000	
E	Solvent	Via 1	30	0.150	0.075	NO
	Dry	Via 1	17	0.000	0.000	
	Solvent	Via 2	26	0.329	0.225	NO
	Dry	Via 2	13	0.216	0.036	

# Summary

- A reliable, cost effective alternative to solvent de-veil processing has been developed.
  - Same or improved yield and device performance
  - Solvent failure mechanisms have been eliminated
  - Process wafer cost is reduced to <15% of the solvent process
- Dry De-veil technology is better for safety and less overall burden to the environment
  - Eliminates hazardous waste disposal
  - Reduces overall DI water consumption
  - Requires less safety equipment
- This via de-veil technology is extendable to other solvent de-veil processes: (i.e. metal etch, poly etch, ion implant, etc.)

